# Degradation of Phenacetin in Wastewater by Electro-Oxidation: Effect

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of Variables and Evaluation of Acute Toxicity

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This study aims to optimize the electro-oxidation (EO) process, to efficiently degrade phenacetin, through a central composite design based on response surface methodology. The process was carried out in a reactor containing 100 mL of solution, with boron-doped diamond (BDD) anode and carbon-PTFE air-diffusion cathode. According to the results, from the analysis of variance, the model presents a good correlation between the observed and predicted values. Thus, under optimal operation conditions (pH = 7.05, *j* = 102 mA cm<sup>-2</sup> and 13 min for degradation and 214 min for mineralization), 65.6% degradation and 51.9% mineralization were achieved. The use of EO-H<sub>2</sub>O<sub>2</sub> process reduced the toxicity, as shown by acute ecotoxicity tests using *Artemia salina*.

## Introduction

In recent years, concern about the impact of pollution from emerging contaminants has focused on conventional pollutants. However, there is a growing interest in investigating another group of substances: pharmaceuticals [1,2]. Phenacetin (PNT, N-(4ethoxyphenyl)-acetamide) is an analgesic, being the first drug successfully synthesized as an antipyretic [3]. Due to its potential carcinogenicity, it was banned in many countries in the 70s [4]. However, it is still permitted in medications in combination with other drugs [5]. Considering that prolonged exposure to phenacetin can pose serious health risks and its removal through conventional treatments has not been effective [6], advanced oxidation process (AOPs), including electro-oxidation (EO), emerges as a promising technology to remove PNT from the environment [7] efficiently. Considering the above premises, the elimination of the PNT in a real effluent was evaluated by the EO-H<sub>2</sub>O<sub>2</sub> process following a central composite design (CCD) 2<sup>3</sup> factorial planning. Additionally, the acute toxicity of the treated solutions was tested using Artemia salina.

# **Material and Methods**

The electrolytic system was an undivided electrochemical cell jacketed for water recirculation at 25 °C. An air-diffusion electrode made of a carbon-PTFE supplied by E-TEK (Somerset, NJ, USA) and a boron-doped diamond (BDD) thin film electrode supplied by NeoCoat (La-Chaux-de-Fonds, Switzerland) were used as cathode and anode, respectively, both with an area of 3 cm<sup>2</sup> and separated by 1 cm. A 100-mL solution of PNT containing 0.05 mol L<sup>-1</sup> Na<sub>2</sub>SO<sub>4</sub> as the electrolyte

was employed for the electrolyses. These solutions were prepared in actual wastewater samples from the up-flow anaerobic sludge blanket (UASB) postreactor effluent (i.e., secondary effluent) from a treatment plant in the municipality of Campo Grande, Brazil. The mineralization was assessed with a Shimadzu TOC-V CPN analyzer. PNT decay was monitored by high-performance liquid chromatography using a Shimadzu SPD-M20A chromatograph with a C18 column and diode array detector. The acute toxicity tests were first conducted with Artemia salina nauplii. A CCD 2<sup>3</sup> was applied to investigate and optimize the system variables applied current, j (60 mA cm<sup>-2</sup> as a central point), pH (5.5 as a central point) and time (8 and 130 min to degradation and mineralization times, respectively, as a central point). A total of 17 experiments were conducted, being distributed as: 8 cube points (levels -1 and +1), 6 axial points (levels -1.63 and +1.63) and 3 replicates at the central point (0). All experimental designs in this work were analyzed using the Minitab 19 statistical software program.

## Results and Discussion

Analysis of variance (ANOVA) was evaluated to determine model fit. This model is highly significant (Table 1), with a p-value = 0.000 for both degradation and mineralization. The high values of the regression coefficients for degradation and mineralization (R<sup>2</sup> of 98.2% and 98.7, respectively) confirm the adequacy of the model. All linear factors were significant for degradation and mineralization. The quadratic terms Time\*Time for degradation and mineralization and the pH\*pH for mineralization were significant,

suggesting that these terms tend to be more effective at intermediate values. The significant interactions for the model were j\*pH and j\*Time for PNT degradation and pH\*Time for mineralization. Using the Minitab Statistical program, the ideal conditions to treat PNT were obtained:  $i = 102 \text{ mA cm}^{-2}$ , pH = 7.05, and reaction time of 13 and 214 min for degradation and mineralization, respectively. Under these conditions, 68.4% of degradation and 47.3% of mineralization are predicted. Triplicate tests were carried out to confirm these conditions, achieving 65.6% and 51.9% for degradation and

### mineralization, respectively.

The toxicity of PNT and its byproducts was evaluated in *Artemia salina* larvae. The toxic effect of the raw effluent and the raw effluent enriched with 25 mg L<sup>-1</sup> of PNT presented a high mortality rate of the organism with a LC50 of 80.5 and 70.8 mg L<sup>-1</sup>, respectively, indicating high toxicity for the test organism. Regarding the treated solutions, no significant acute toxicity was observed.

Table	1. ANOVA	results	for PNT	removal by	/ FO-H <sub>2</sub> O <sub>2</sub>	process
rable	I. ANOVA	results		removarby		process.

Source		Degrada	tion	Mineralization		
Source	(%)	F-value	p-value	(%)	F-value	p-value
Model	98.2	41.7	0.000	98.7	57.1	0.000
Linear	86.5	110.3	0.000	82.2	142.7	0.000
j	21.9	83.5	0.000	20.5	107.0	0.000
рН	4.8	18.5	0.004	18.5	96.2	0.000
Time	59.8	228.7	0.000	43.2	225.0	0.000
Interaction	5.6	7.1	0.016	3.1	5.4	0.031
<i>j</i> *pH	3.5	13.2	0.008	0.8	4.0	0.084
<i>j*</i> Time	2.0	7.5	0.029	0.2	0.9	0.386
pH*Time	0.1	0.5	0.510	2.1	11.2	0.012
Quadratic	6.1	7.8	0.012	13.4	23.3	0.001
j*j	2.1	2.2	0.179	0.2	3.8	0.091
pH*pH	0	0.9	0.371	8.3	60.3	0.000
Time*Time	4.0	15.4	0.006	4.9	25.6	0.001
Lack of fit	1.3	1.1	0.545	1.2	3.0	0.271
Error	1.8			1.3		
Summary	<i>R</i> <sup>2</sup> = 98	.2%; <i>R</i> <sup>2</sup> <sub>Adj</sub> = 95.8	%	$R^2 = 98$	.7%; $R^2_{Adj} = 96$ .	9%

### Conclusions

The effectiveness of the  $EO-H_2O_2$  process for eliminating PNT in real wastewater was confirmed by the 100% removal of 25 mg L<sup>-1</sup> of the drug after 90 min under optimized conditions, along with a high mineralization percentage after 300 min. The treated solutions reduced the toxicity and showed promising results for the remediation of PNT residues in wastewater.

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